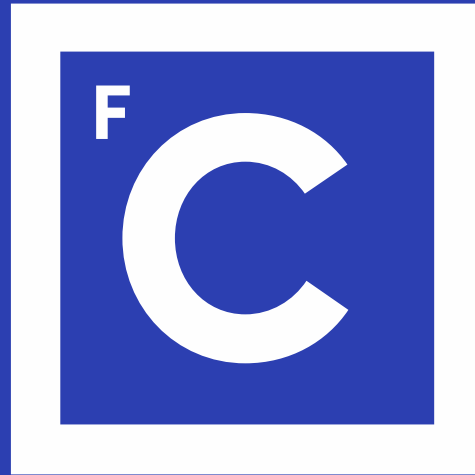




Ciências ULisboa

Faculdade
de Ciências
da Universidade
de Lisboa

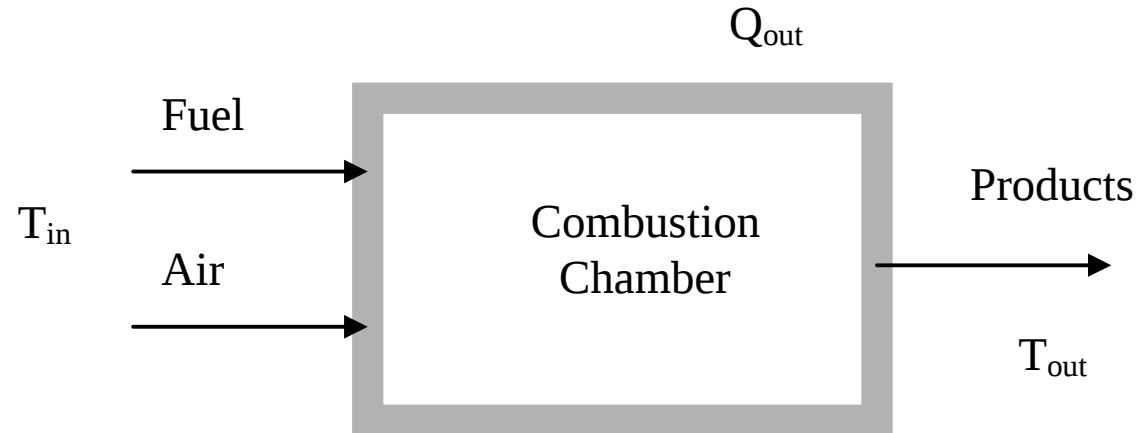
DISCIPLINA MIEA 2018



Technologies of combustion

Corpo docente

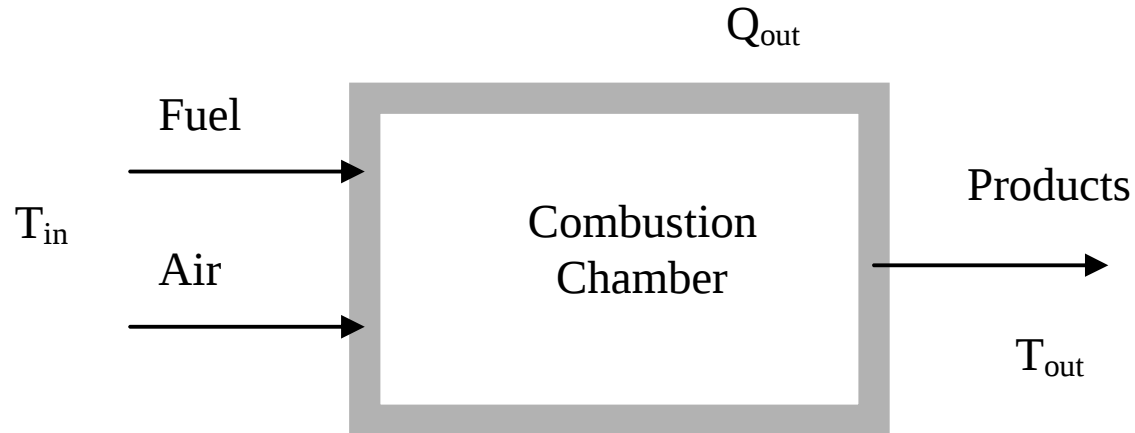
Carla Silva (Teóricas e práticas) /Theory and practice
camsilva@ciencias.ulisboa.pt



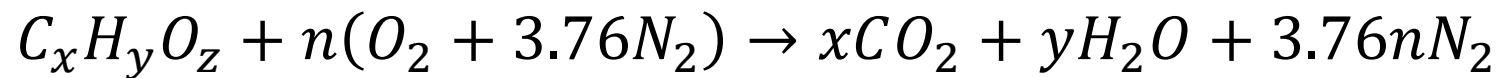
- Maximum heat release, $\max Q_{out}$: $T_{out}=T_{in}$
- Maximum flame temperature, T_{ad} :

$H_{reag}(T_{in})=H_{prod}(T_{ad})$ (constant pressure, e.g. Diesel engine, gas turbine, furnace)

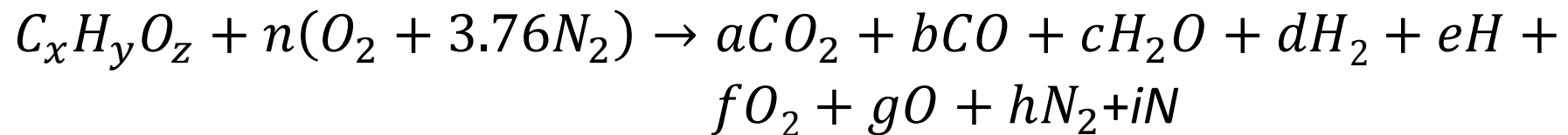
$H_{reag}(T_{in})=H_{prod}(T_{ad})-R(n_{prod}T_{ad}-n_{reag}T_{in})$ (constant volume, e.g. gasoline engine)

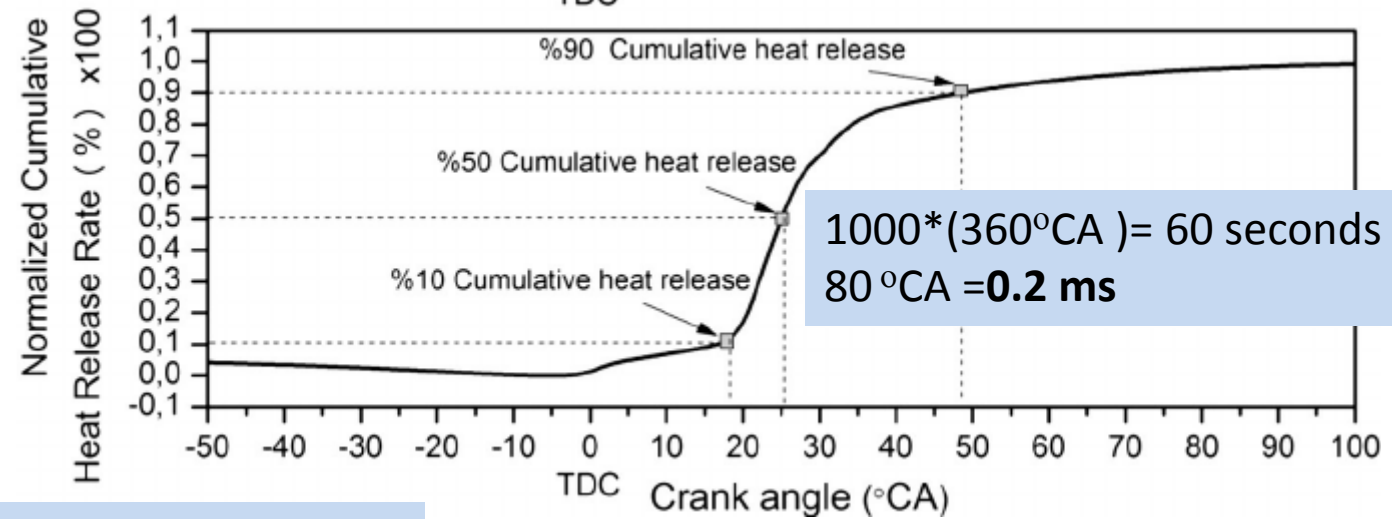
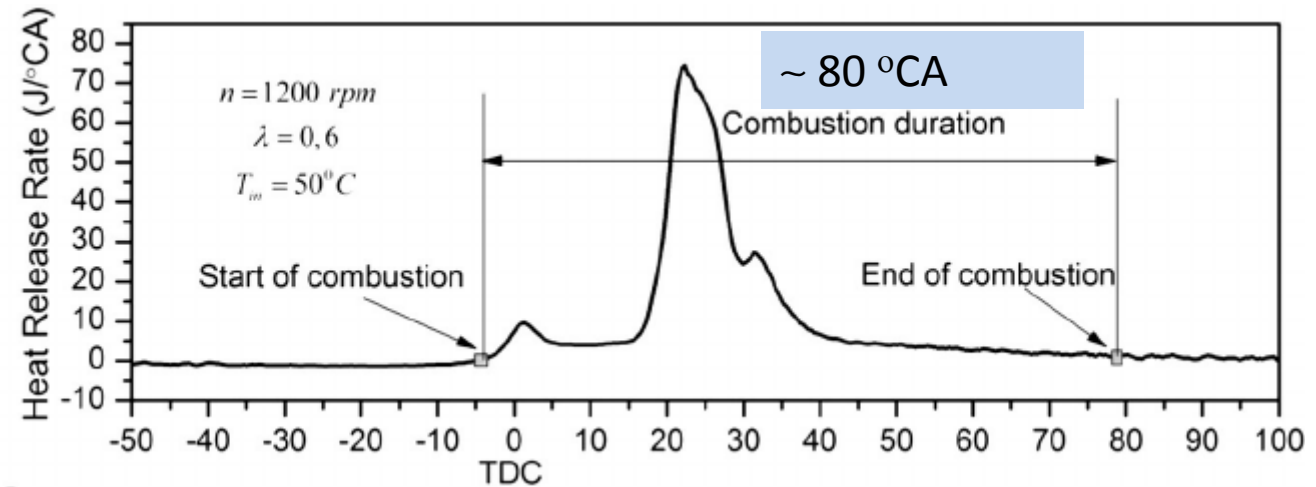
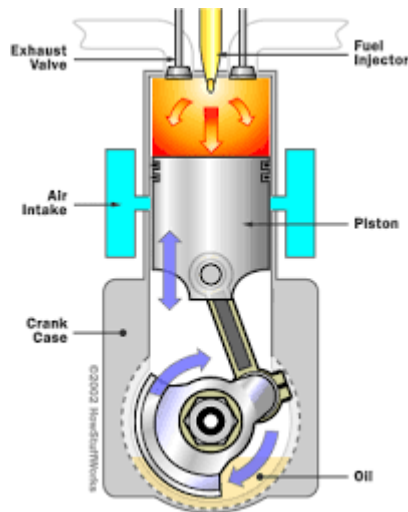


- Ideal stoichiometric combustion

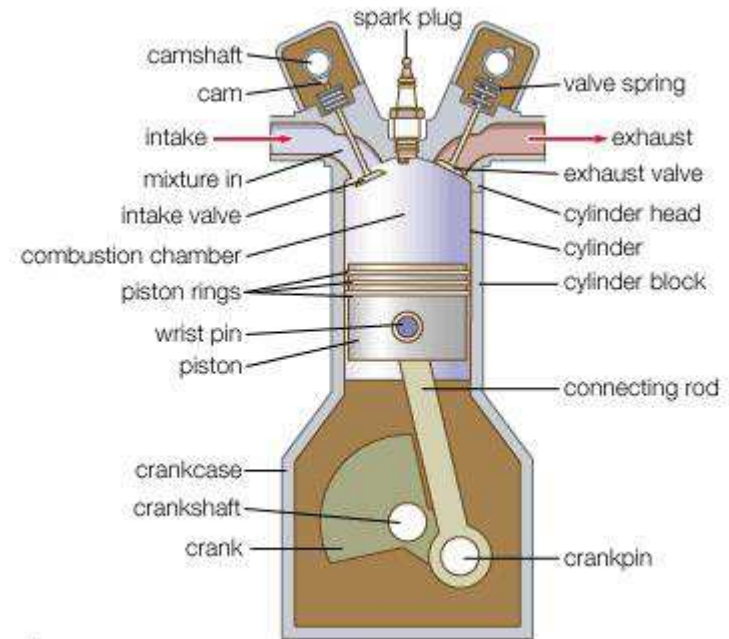
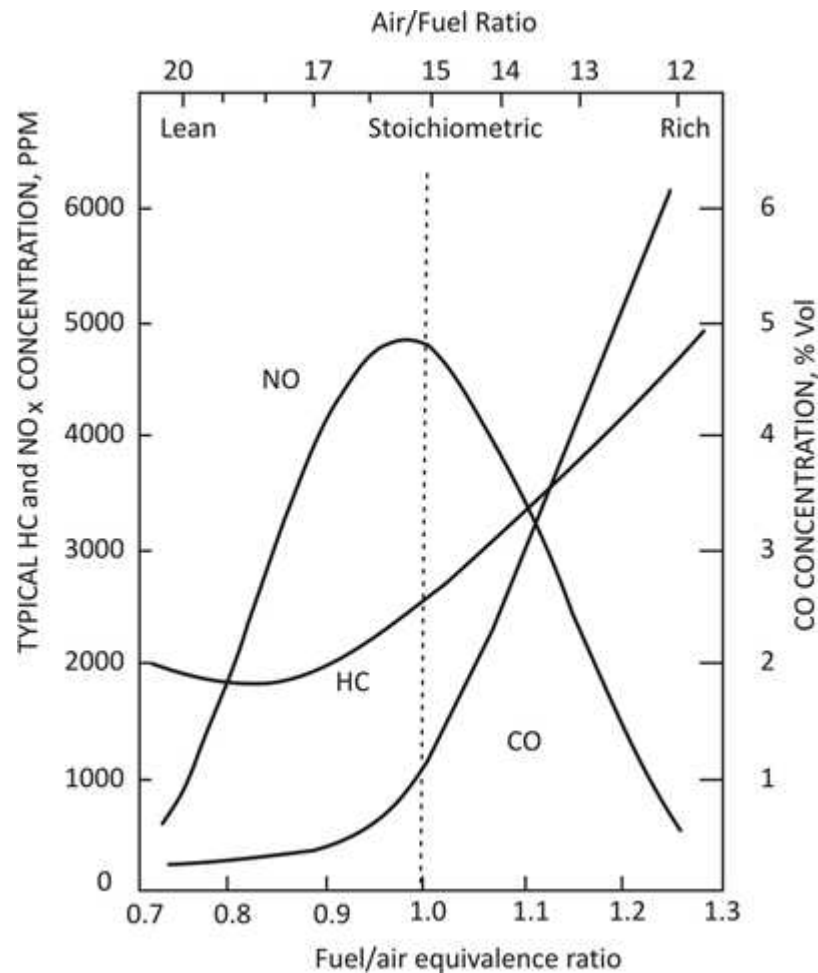


- Real stoichiometric combustion



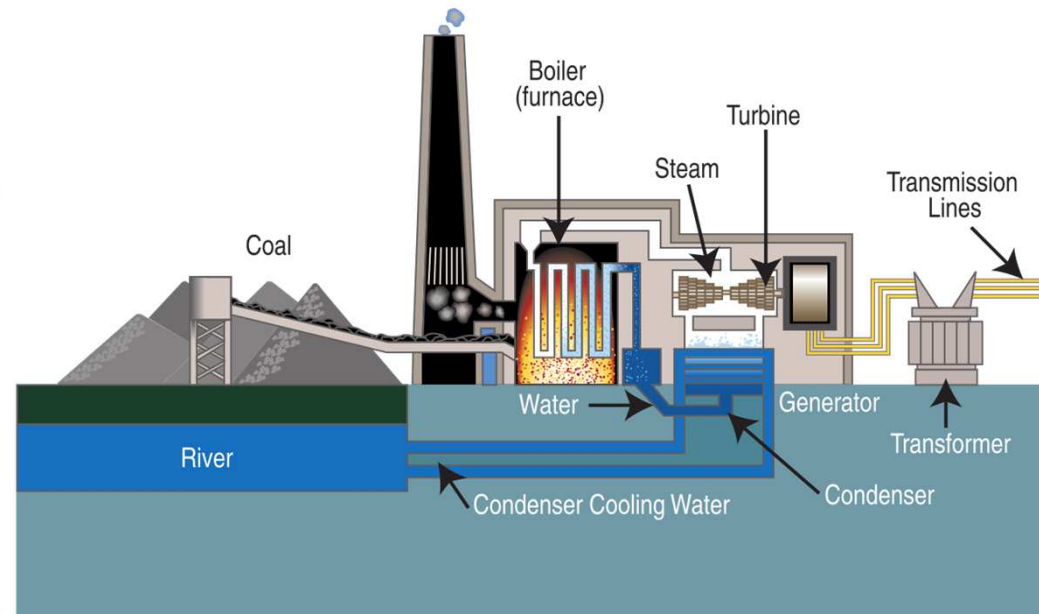
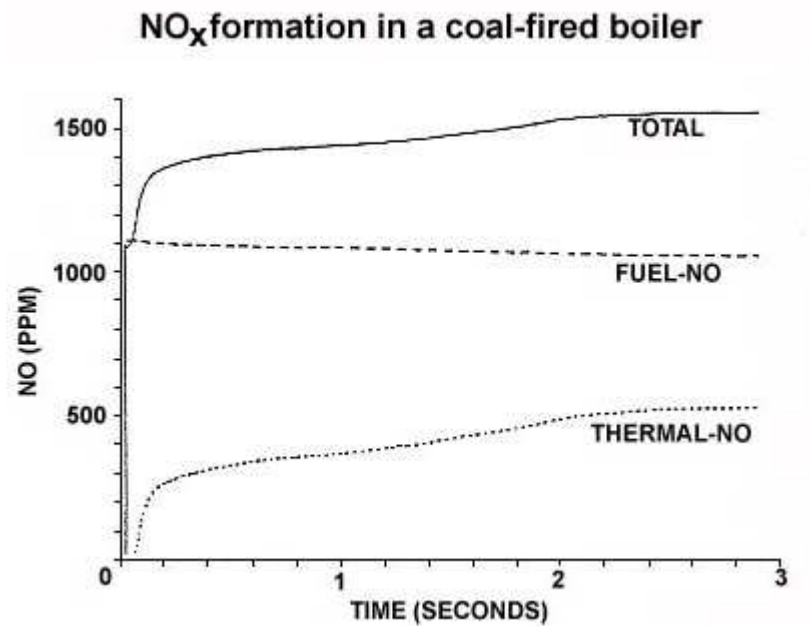


More rpm, less combustion time!!!



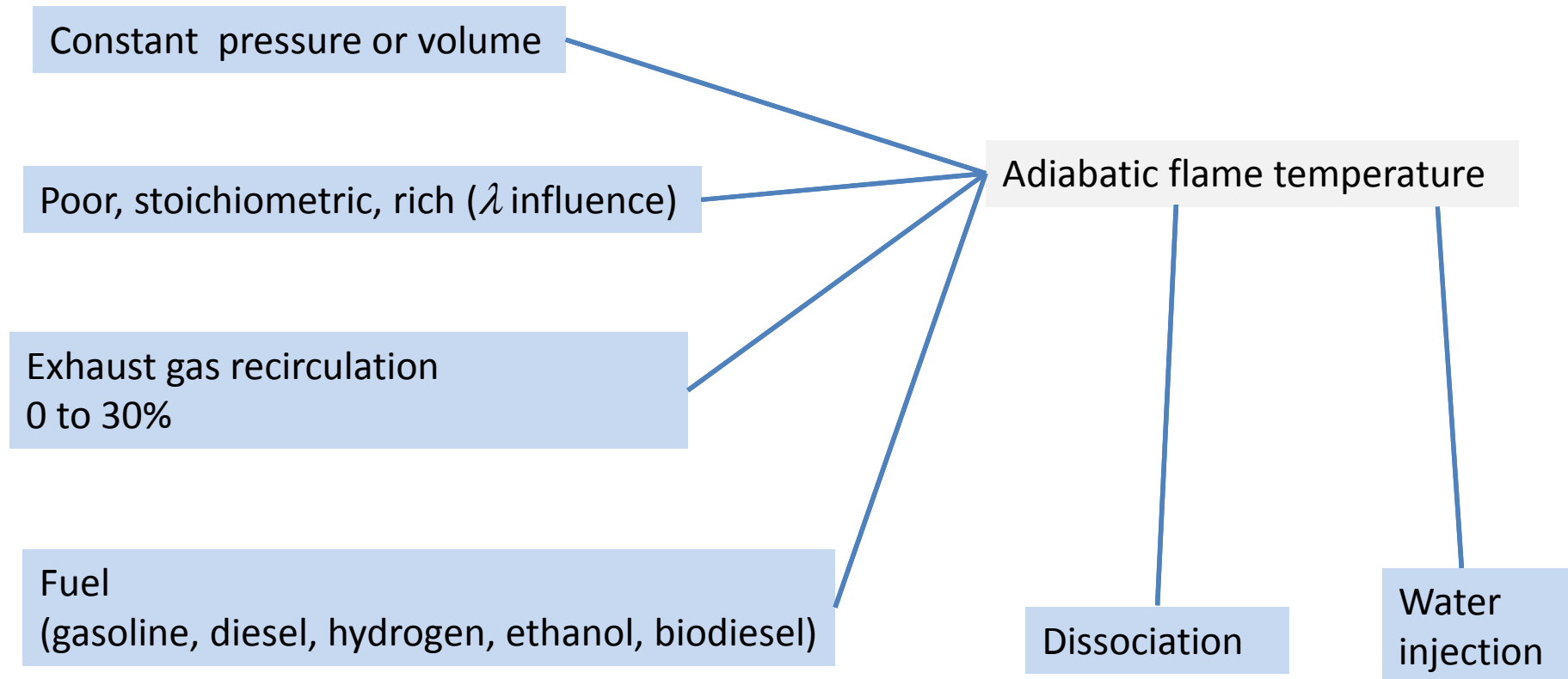
© 2007 Encyclopædia Britannica, Inc.

$$\phi = \frac{1}{\lambda}$$



ppm ☺ !!!!

Adiabatic Flame Temperature



low emission zones and the raising of air-quality target



particulate matter (PM)
ozone (O₃)
nitrogen dioxide (NO₂)
sulfur dioxide (SO₂)

Ambient (outdoor air pollution) in both cities and rural areas was estimated to cause **3 million** premature deaths worldwide in 2012

Emissions-Outdoor sources



Stationary combustion
(limits in mg/m³)



Mobile combustion
(limits in g/km)

low emission zones and the raising of air-quality target

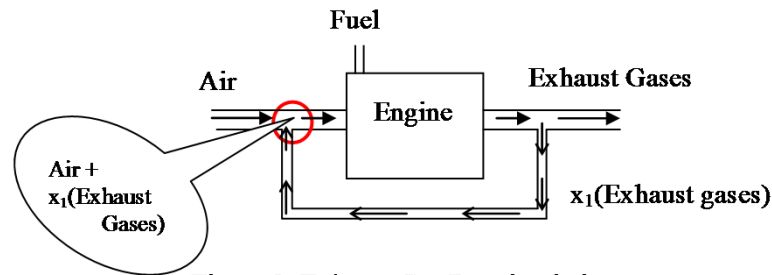
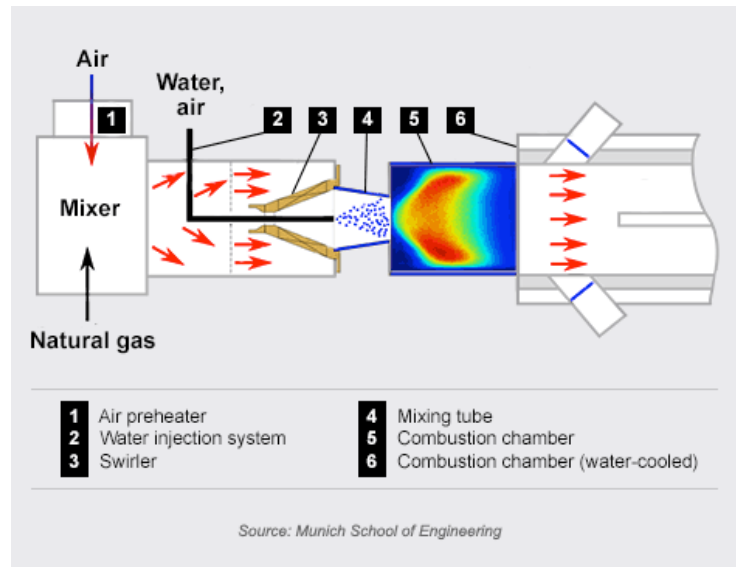


Figure 2: Exhaust Gas Re-circulation

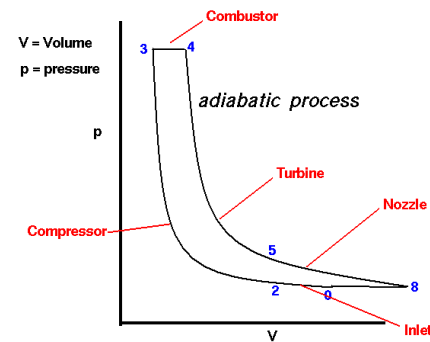
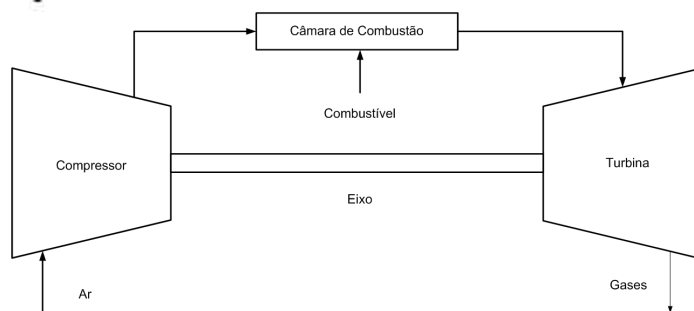
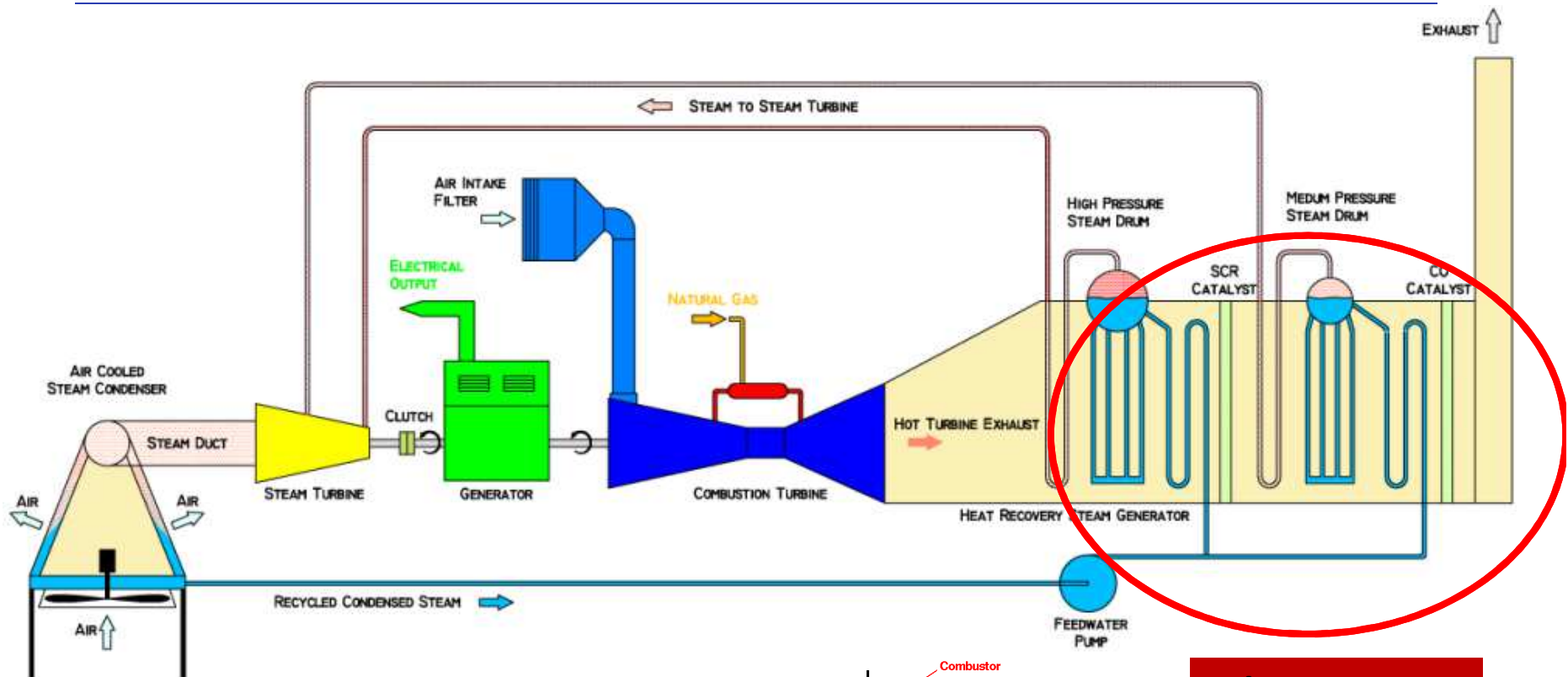
Combustion alteration not enough!!!!



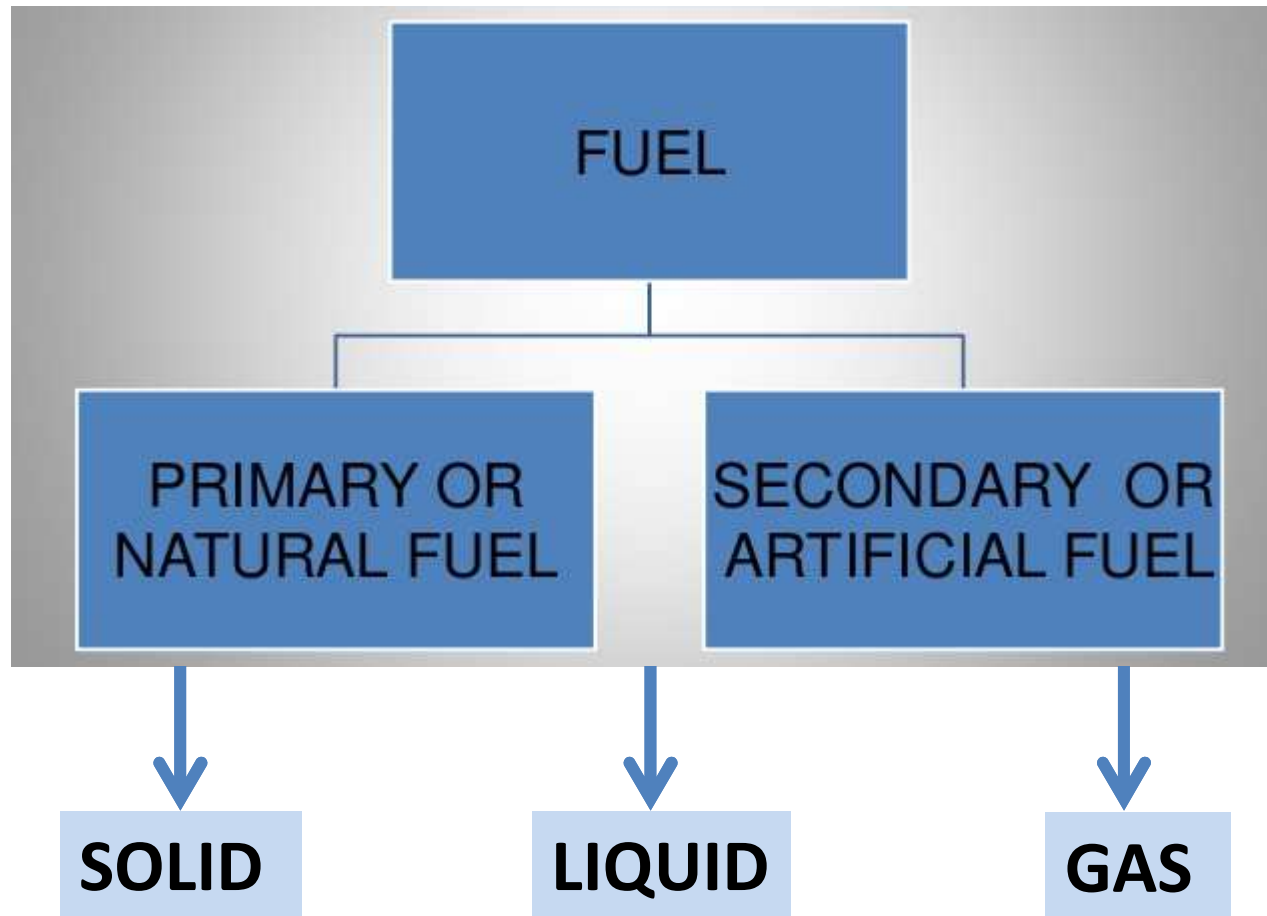
CO_2
 H_2O
 N_2
 CO
 HC
 NO
 NO_2
 PM

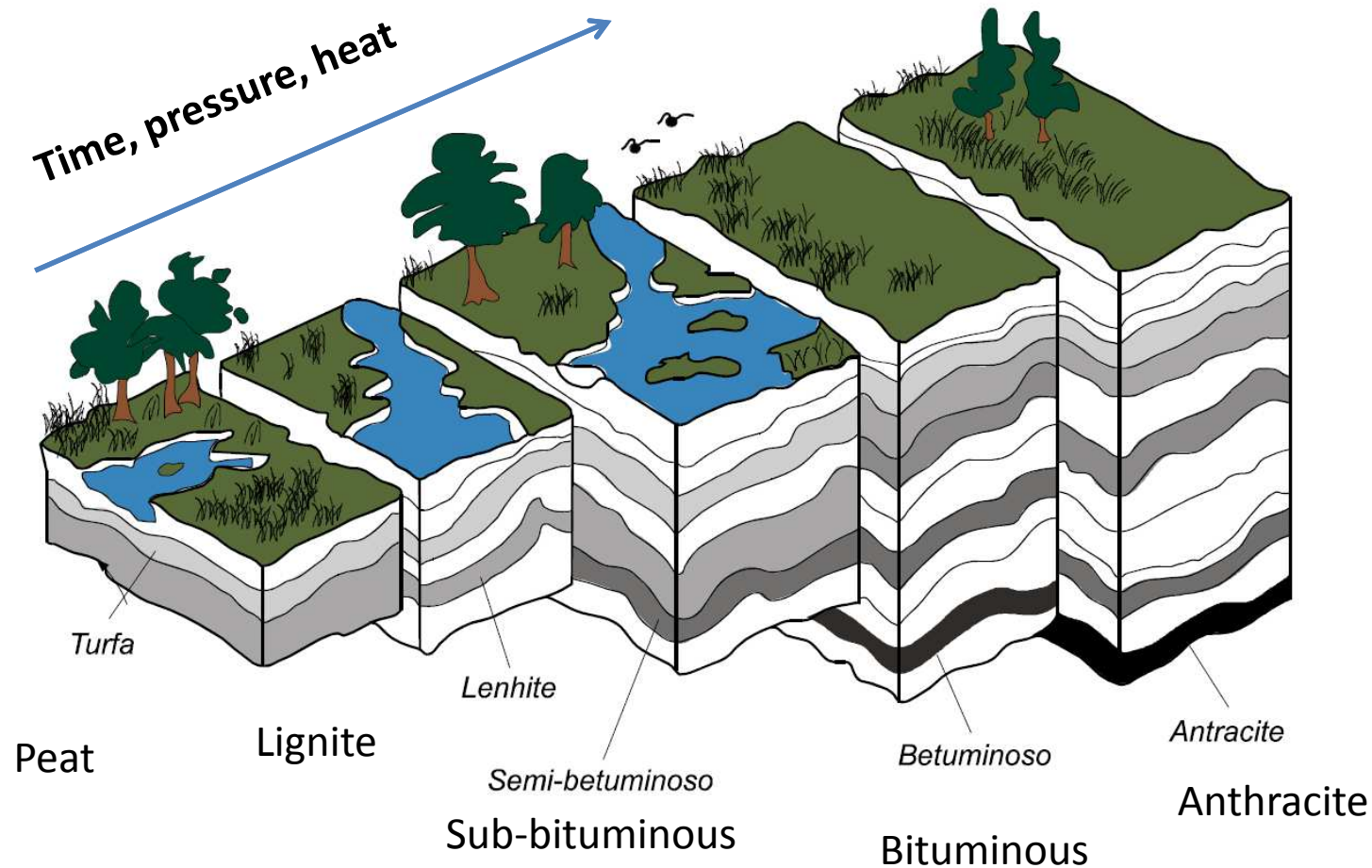
→ **Exhaust gas aftertreatment** →

CO_2
 H_2O
 N_2



**Exhaust gas
aftertreatment**





Time, pressure, heat



Peat

Lignite

Sub-bituminous

Bituminous

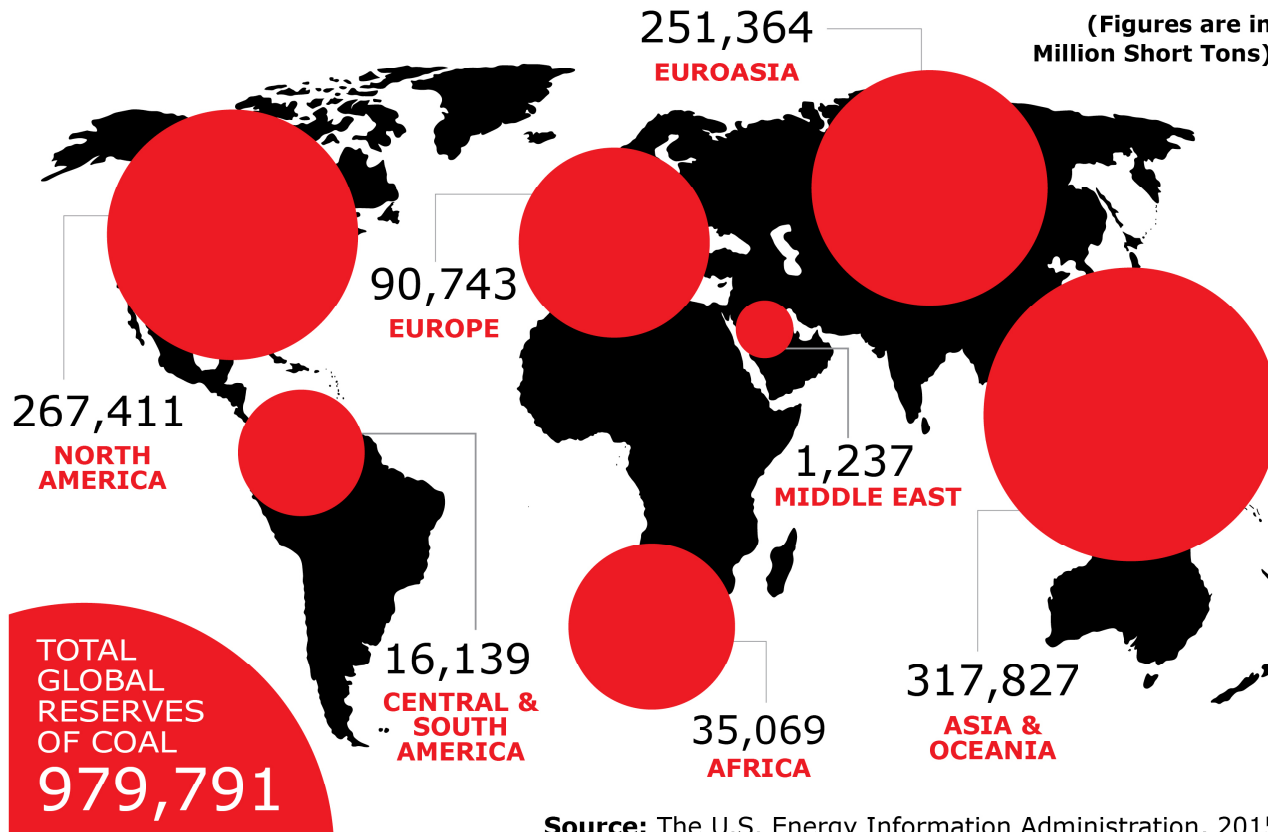
Anthracite

WORLD COAL RESERVES BY REGION

Coal reserves are available in almost every country. The biggest reserves are in the Asia & Oceania region.



(Figures are in
Million Short Tons)

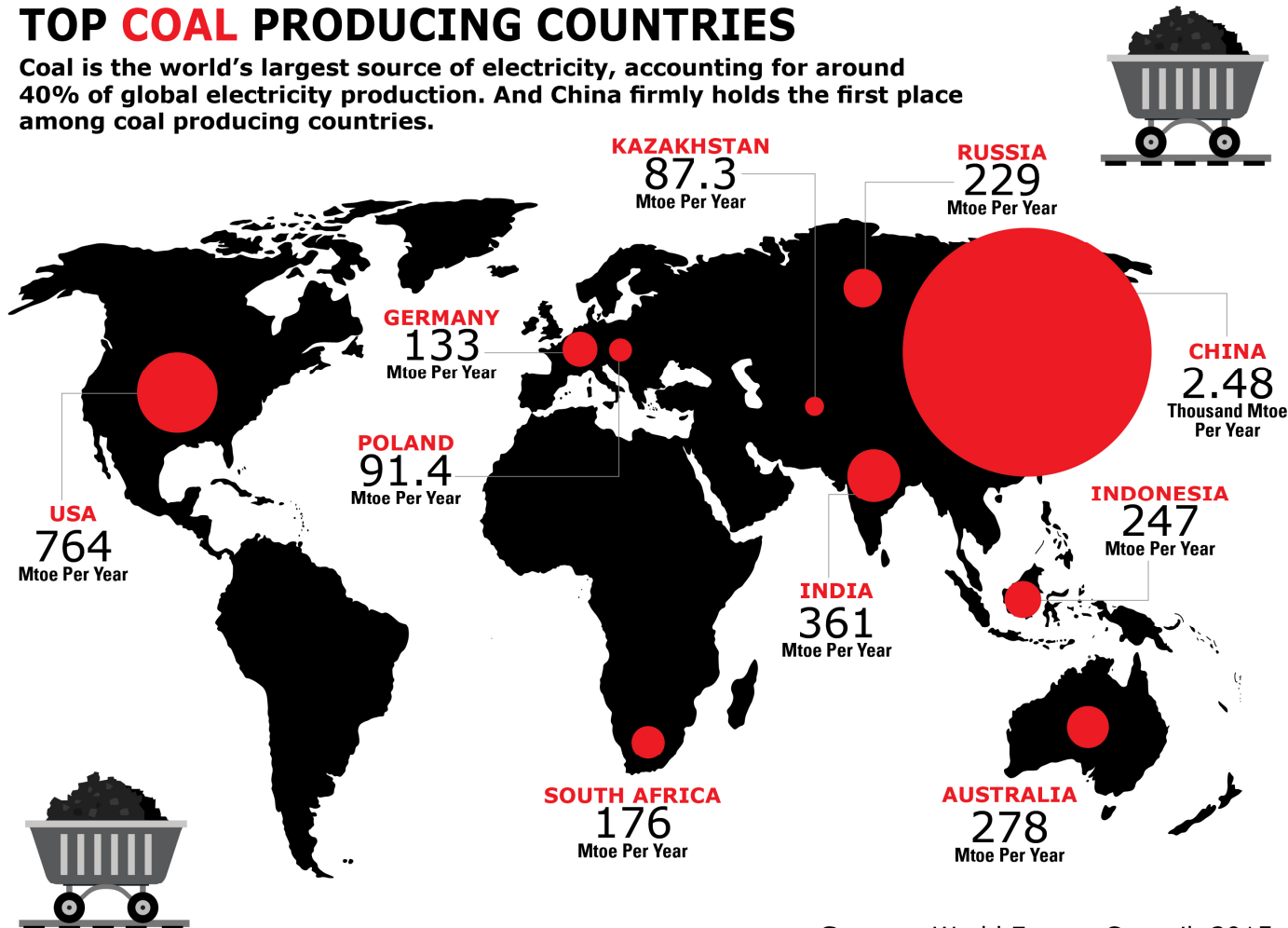


1 short ton
907.18474 kg

Source: The U.S. Energy Information Administration, 2015

TOP COAL PRODUCING COUNTRIES

Coal is the world's largest source of electricity, accounting for around 40% of global electricity production. And China firmly holds the first place among coal producing countries.



Source: World Energy Council, 2015

A composição é caracterizada por dois tipos de análise

- Análise Elementar
- Análise Imediata

Análise Elementar - Frações mássicas dos elementos:

C, H, O, N, S e cinzas (atualmente inclui-se Cl, Ca, ...)
Azoto (NP1012), Enxofre (ASTM D3177)

Análise Imediata - Frações mássicas de acordo com decomposição:

Humidade (determinada a 110°C)
Matéria volátil (gases libertados em aquecimento a 950°C) - NP3423
Carbono fixo (obtido por diferença para os restantes valores)
Cinza (matéria restante após oxidação do resíduo carbonoso) - NP1019

Table 1.7 Relationship Between Ultimate Analysis and Proximate Analysis			
	%C	=	$0.97C + 0.7(VM - 0.1A) - M(0.6 - 0.01M)$
	%H	=	$0.036C + 0.086(VM - 0.1xA) - 0.0035M^2(1 - 0.02M)$
	%N ₂	=	$2.10 - 0.020 VM$
where			
	C	=	% of fixed carbon
	A	=	% of ash
	VM	=	% of volatile matter
	M	=	% of moisture

A entalpia de formação do carvão é próxima de zero

Tipo de carvão	Carbono % massa	Hidrogénio % massa	Idade (anos*10 ⁶)
Antracites	93 - 95	3.8 - 2.8	210 - 250
Carbonoso*	91 - 93	4.25 - 3.8	210 - 250
Bituminoso*	80 - 91	5.6 - 4.35	150 - 180
Sub-bitum.*	75 - 80	5.6 - 5.1	60 - 100
Lenhite	60 - 75	5.7 - 5.0	20 - 60
Turfa	50 - 60	6.1 - 5.8	1
Madeira**	46 - 51	6.2 - 5.9	0

* Hulhas

** Madeira é considerada renovável (não fóssil)

Correlations for Higher Heating Value (HHV or PCS)

$$\text{PCS} \sim 33,8 \, xC + 144,3 (xH - xO/8) + 9,4 \, xS \text{ (Dulong)}$$

$$\text{PCS} \sim 34,1 \, xC + 132,3 [xH - (xO + xN)/11] + 6,8 \, xS - 1,5 \, xAs$$

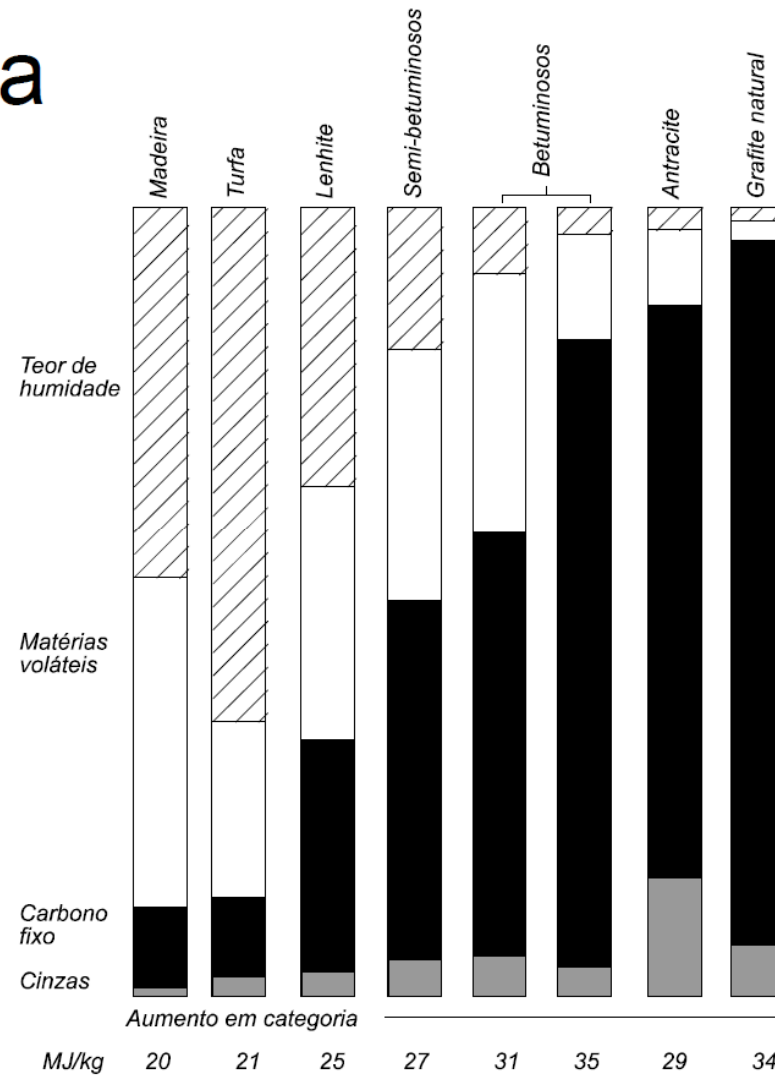
(Mason and Gandhi, 1983)

in MJ·kg⁻¹ and dry basis. Last includes ash effects xAs

Análise Imediata

Nesta análise caracteriza-se a composição do combustível em:

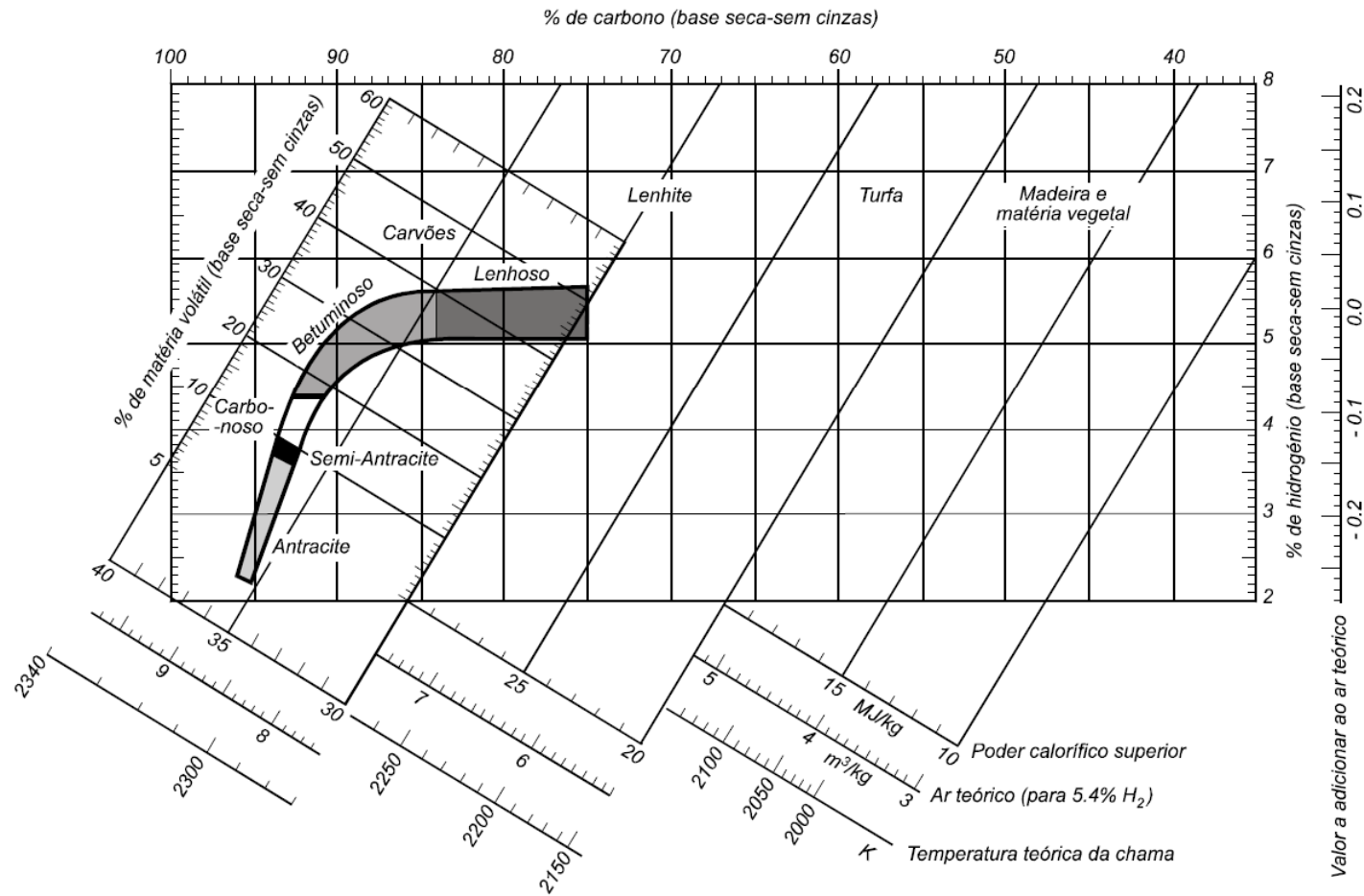
- Humidade
- Voláteis
- Carbono fixo
- Cinzas



A composição dos combustíveis sólidos para ambas as análises pode ser expressa em três bases:

- As received* (A_r - incluindo humidade e cinzas)
- Dry basis* (D_b - base seca, exclui a humidade)
- Dry ash free* (D_{af} - exclui humidade e cinzas)

Diagrama de Seyler (adaptado)



Even with complete combustion the minimum particle emissions are limited by the ash content initially in the fuel



Ash is the general term used to describe the **inorganic** matter in a fuel, e.g. Fe, Ca, K, Si, etc

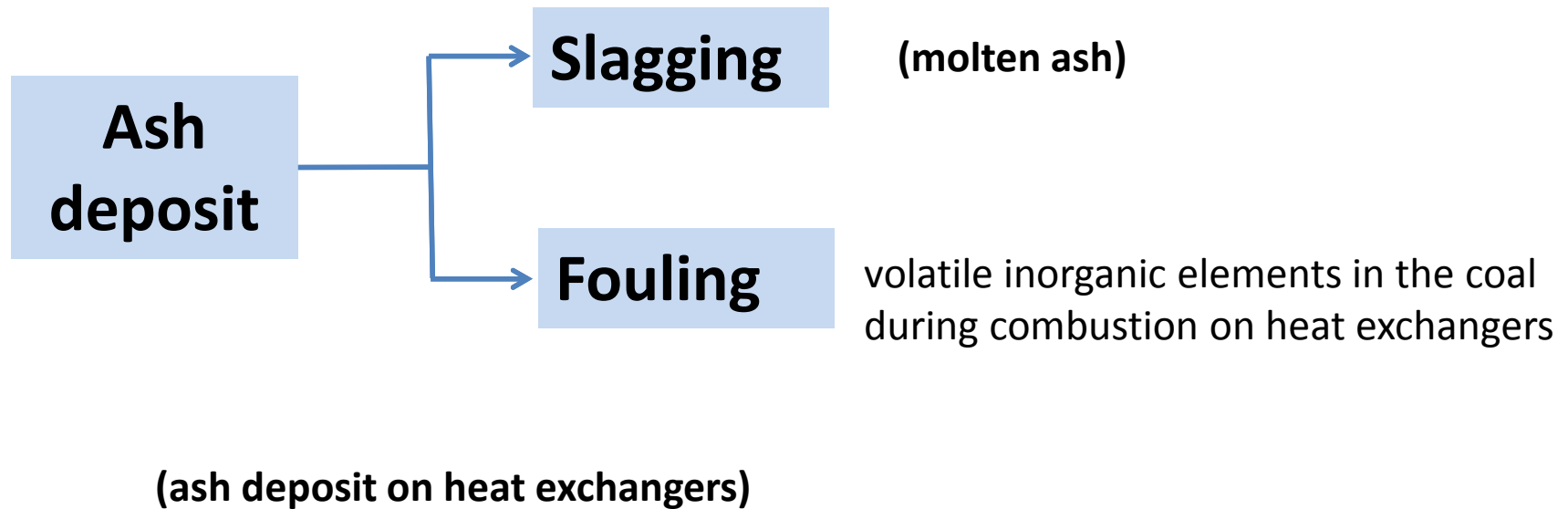


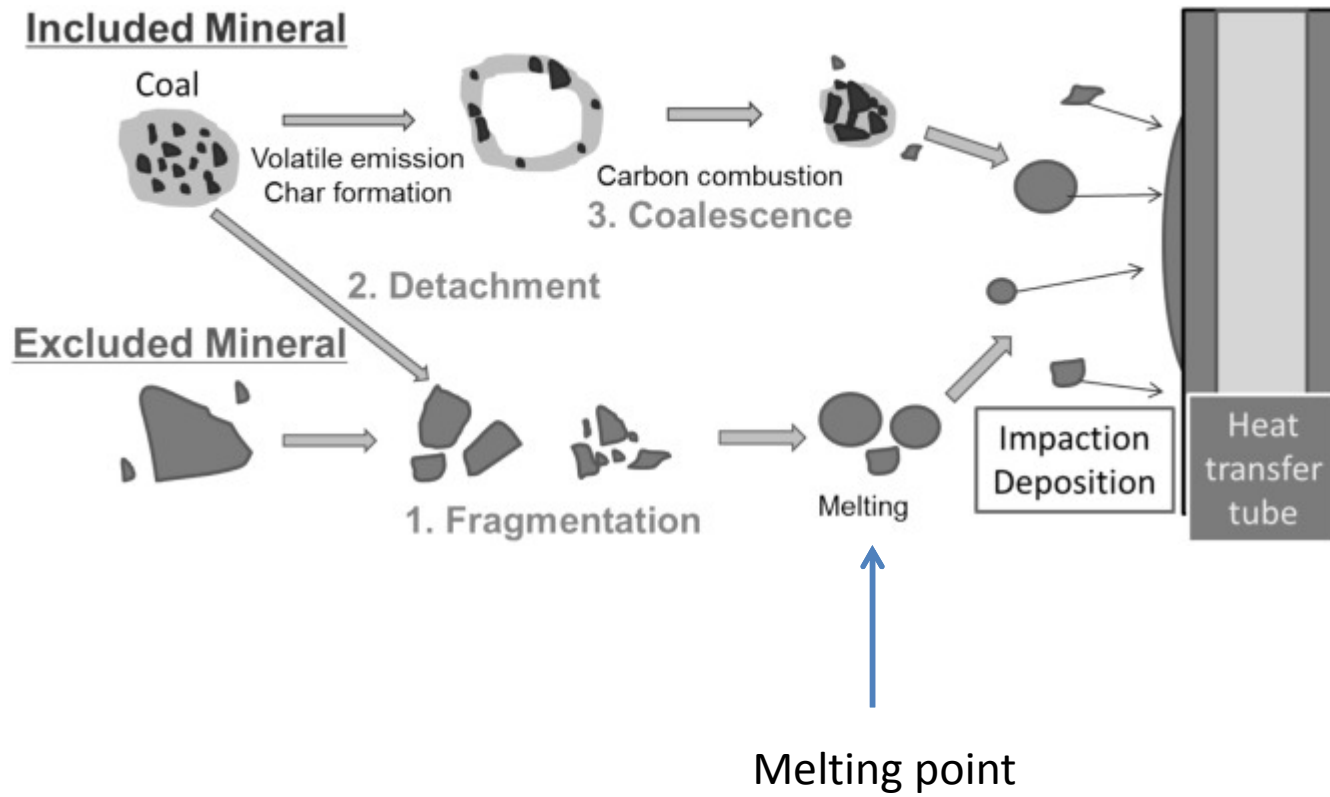
- There is an absence of carbon in its composition
- It is of a non-biologic origin

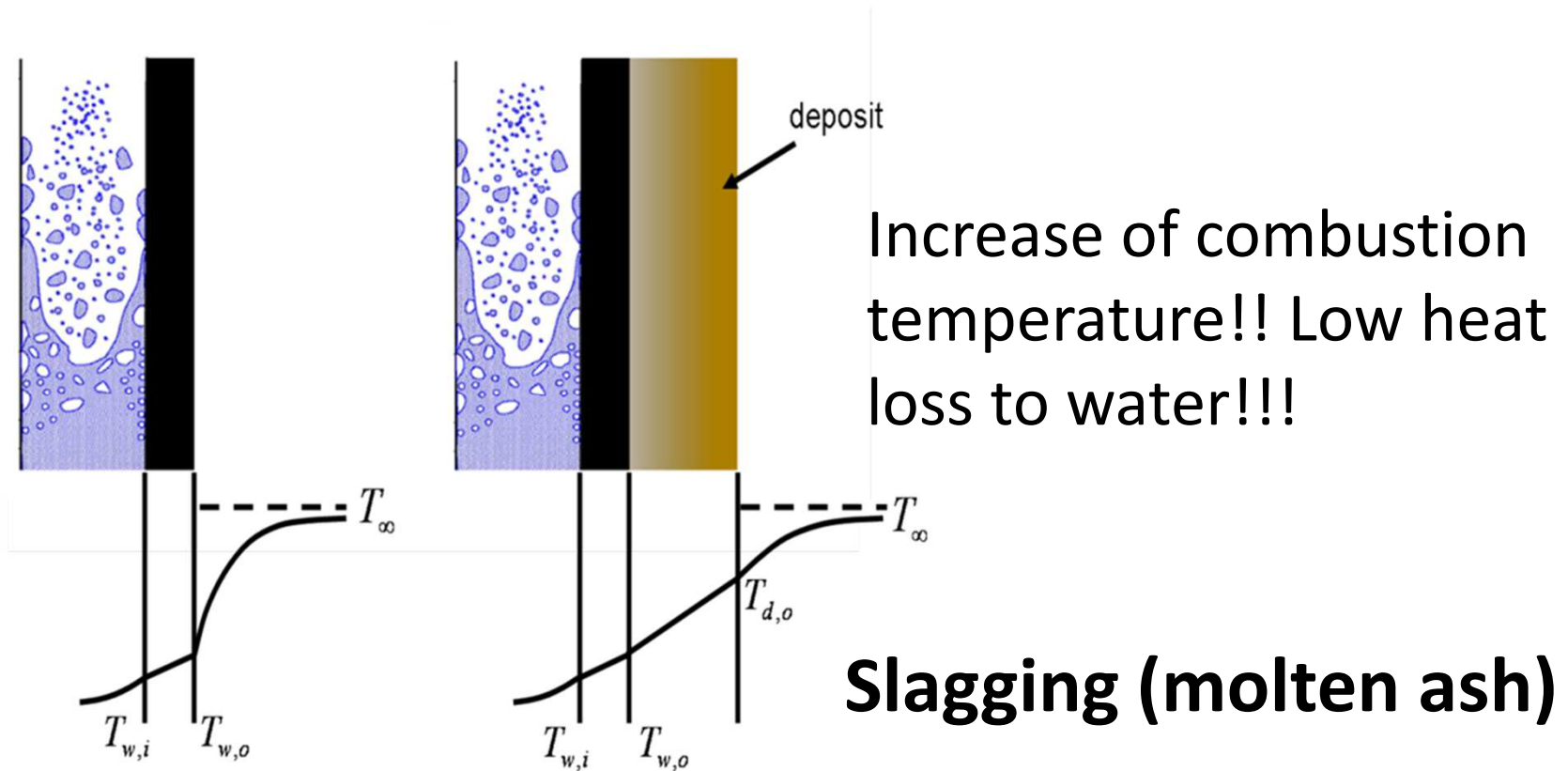
P#12 Consider this coal. Classify the coal according to the Seyler diagram. Identify lower heating value and adiabatic temperature.

Coal composition by weight (%wt). Ash is the general term used to describe the inorganic matter in a fuel, e.g. Fe, Ca, K, Si, etc. Fixed carbon is 51% (volatile matter+fixed carbon+ash+moisture=100%). Moisture is water.

C	67.7
H	4.4
N	1.5
S	1.0
O	5.2
Ash	13.4







Fe-iron Melting temperature: 1538 °C (1811 K)

Magnesium: 650 °C (923 K)

SiO₂ (silica): 1710 °C (1983 K)

Al₂O₃=2072 °C (2345 K)



TABLE 1.5 TYPICAL PROXIMATE ANALYSIS OF VARIOUS COALS (IN PERCENTAGE)			
Parameter	Indian Coal	Indonesian Coal	South African Coal
Moisture	5.98	9.43	8.5
Ash	38.63	13.99	17
Volatile matter	20.70	29.79	23.28
Fixed Carbon	34.69	46.79	51.22

Problems with ash

Biomass	Ash content (%)	Biomass	Ash content (%)
Corn cob	1.2	Coffee husk	4.3
Jute stick	1.2	Cotton shells	4.6
Sawdust (mixed)	1.3	Tannin waste	4.8
Pine needle	1.5	Almond shell	4.8
Soya bean stalk	1.5	Areca nut shell	5.1
Bagasse	1.8	Castor stick	5.4
Coffee spent	1.8	Groundnut shell	6.0
Coconut shell	1.9	Coir pith	6.0
Sunflower stalk	1.9	Bagasse pith	8.0
Jowar straw	3.1	Bean straw	10.2
Olive pits	3.2	Barley straw	10.3
Arhar stalk	3.4	Paddy straw	15.5
Lantana camara	3.5	Tobacco dust	19.1
Subabul leaves	3.6	Jute dust	19.9
Tea waste	3.8	Rice husk	22.4
Tamarind husk	4.2	Deoiled bran	28.2



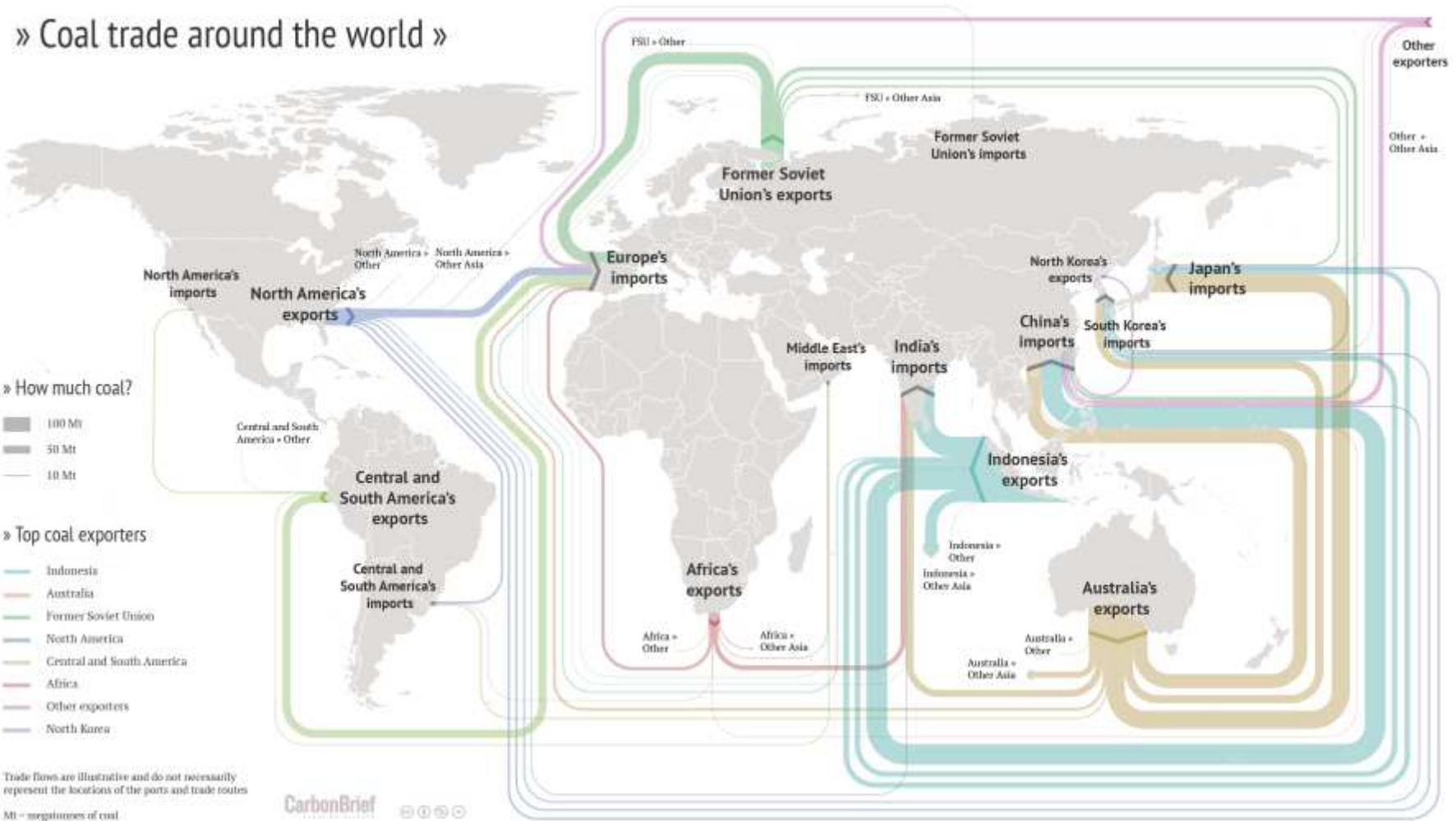


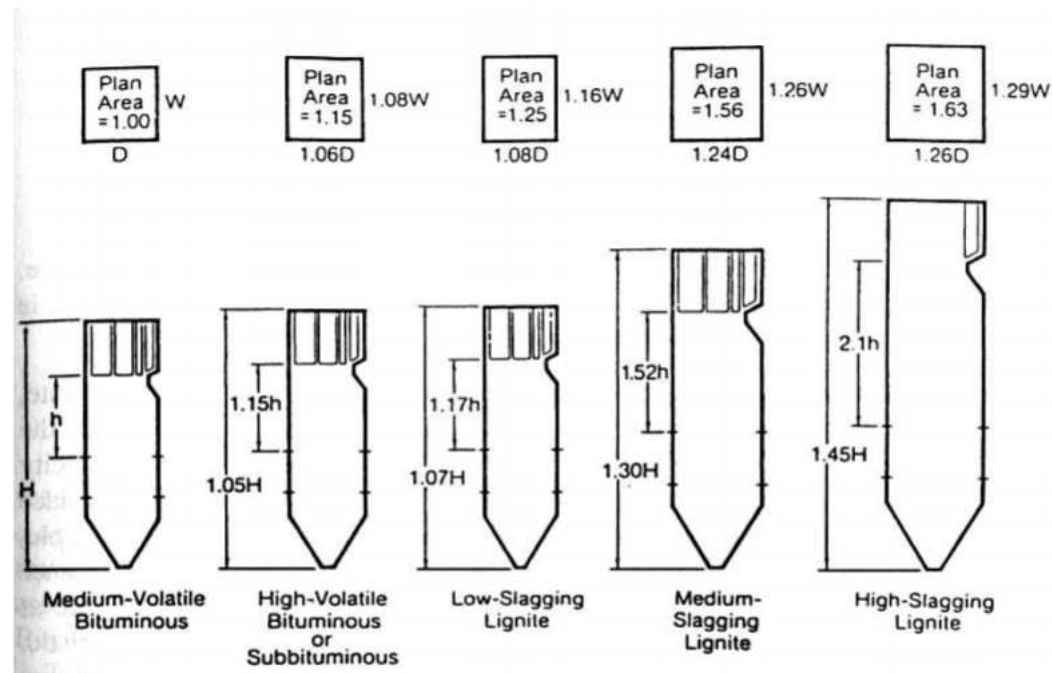
Table 4. Physical and chemical analysis of the coals of the Far East (Vdovichenko V. S et.al, 1991g)

<i>Continent</i>			<i>Eurasia</i>		
<i>Location</i>			<i>Far East (Primorsk region)</i>		
<i>Basin Name</i>			<i>Uglovskiy</i>		
<i>Deposit Name</i>			<i>Artemovskiy</i>	<i>Shkotovskiy</i>	<i>Tavrichanskiy</i>
<i>Proximate Analysis</i>	Moisture, 105°C	wt%, a.r.	23	37	20
	Volatiles, 900°C	wt%, dry	30	35	28.8
	Ash content, 815°C	wt%, dry	40	30	40
	Fixed carbon	wt%, dry	30	35	31.2
<i>Ultimate analysis</i>	Carbon	wt%, dry	40.2	48.65	42.3
	Hydrogen	wt%, dry	3.36	3.85	3.48
	Nitrogen	wt%, dry	0.78	1.05	1.2
	Sulphur	wt%, dry	0.4	0.3	0.5

**Coal low moisture; low ash
the better!!**



Amount of flue gas, burning rate of fuel and slagging propensity also affects the furnace volume



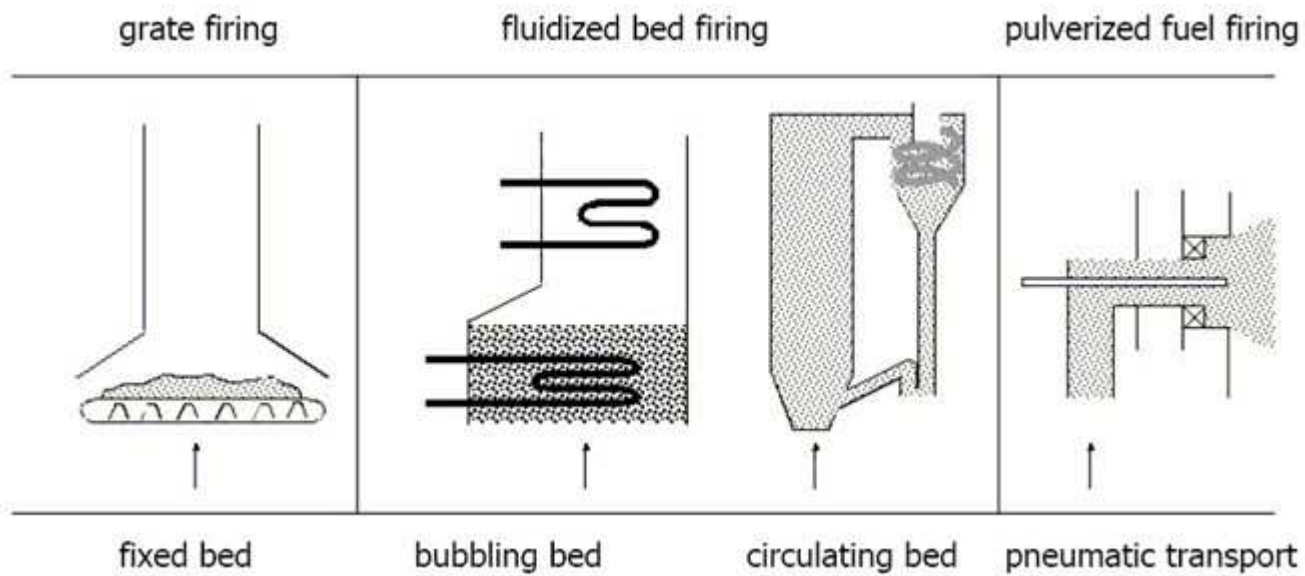


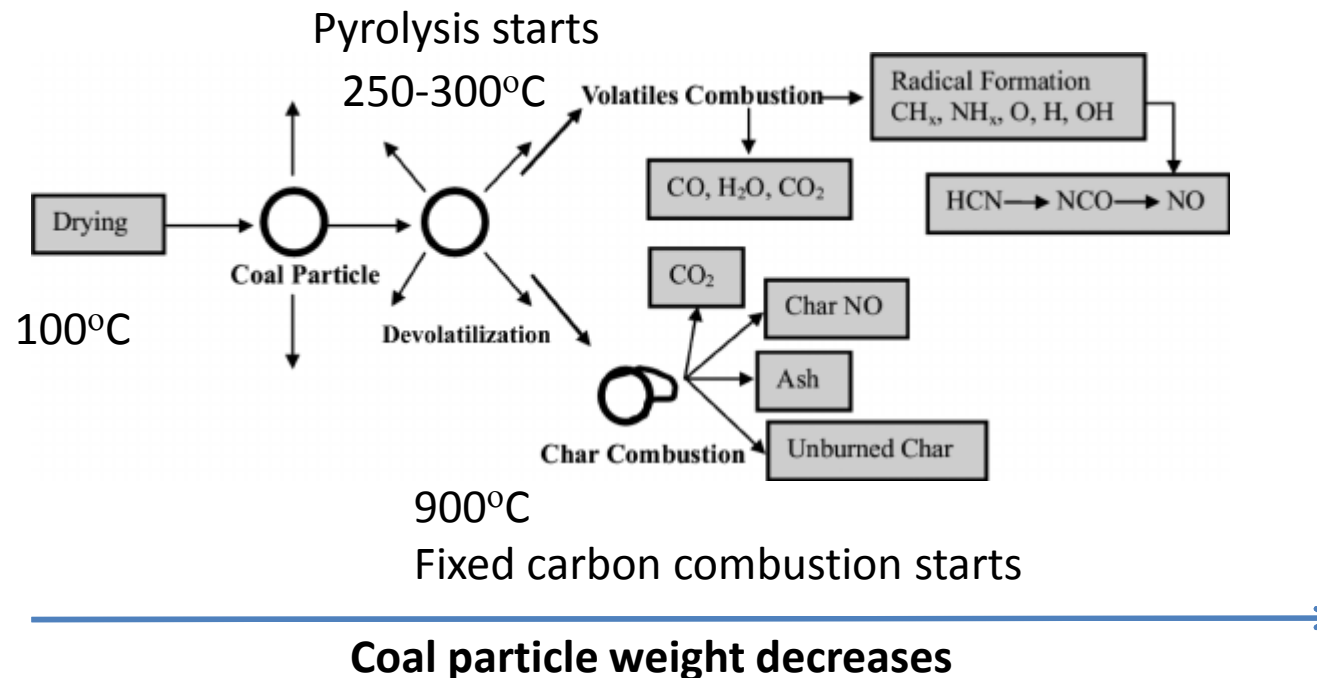
Table 1.8 Proper Size of Coal for Various Types of Firing System		
S. No.	Types of Firing System	Size (in mm)
1.	Hand Firing (a) Natural draft (b) Forced draft	25-75 25-40
2.	Stoker Firing (a) Chain grate i) Natural draft ii) Forced draft (b) Spreader Stoker	25-40 15-25 15-25
3.	Pulverized Fuel Fired	75% below 75 micron*
4	Fluidized bed boiler	< 10 mm

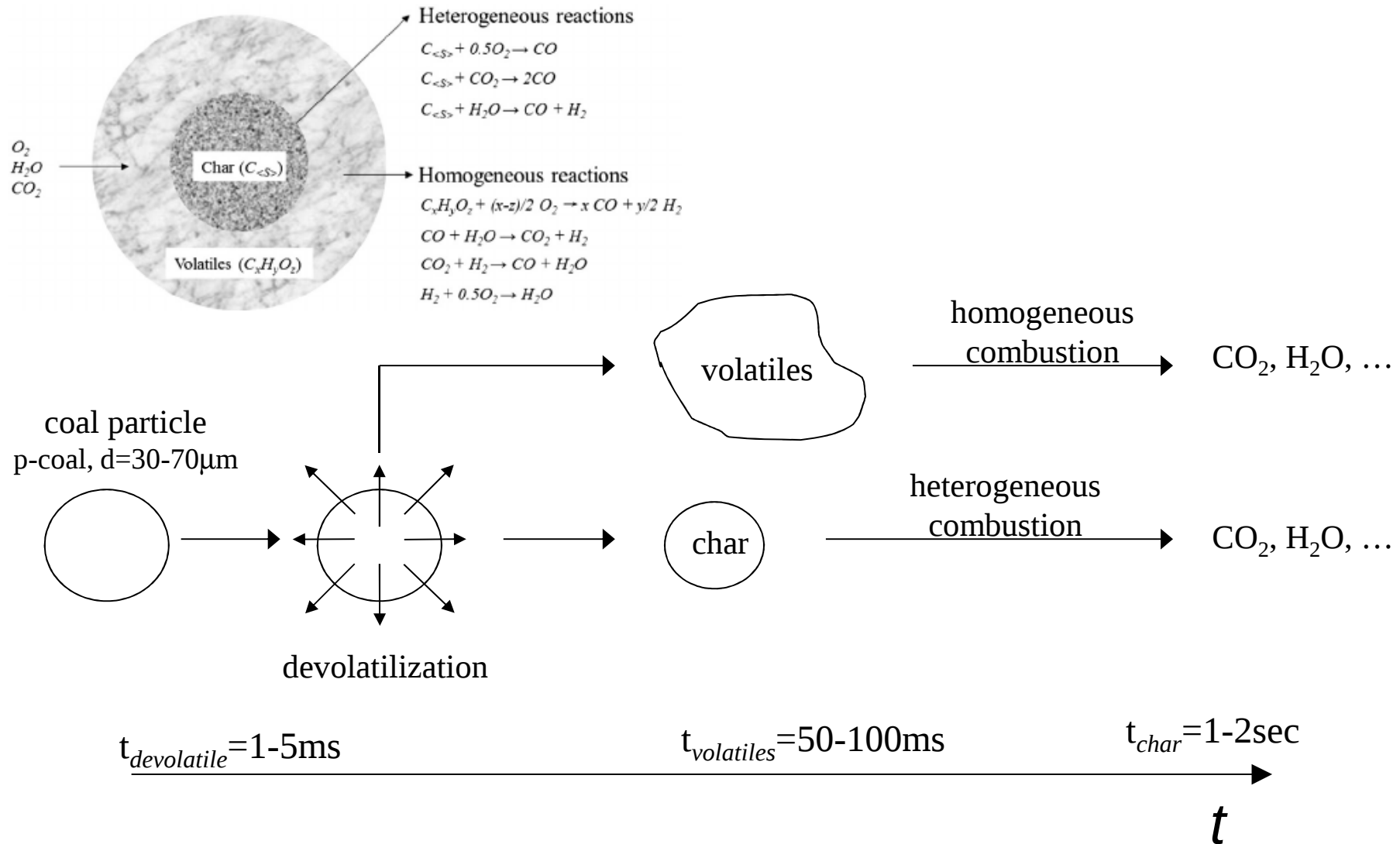
*1 Micron = 1/1000 mm

Combustion in solids

Three stages of mass loss:

- Drying (removal of water): endothermic;
- Devolatilization: vaporization of volatile organic compounds, gas-phase diffusion flames;
- Char combustion: heterogeneous (solid phase fuel, gas phase oxidizer) combustion of fixed carbon.





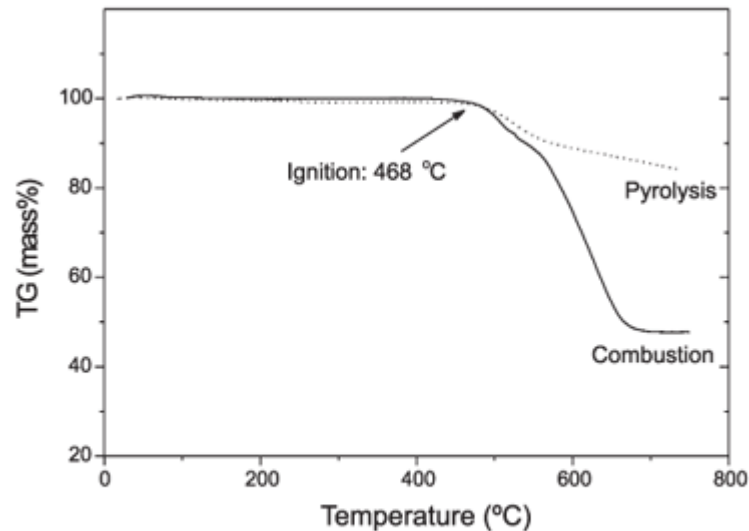


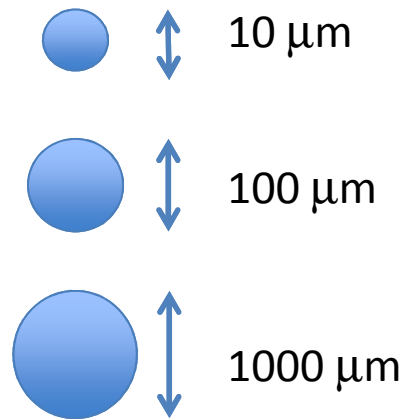
Figure 2. TG results for pyrolysis and combustion of the coal used for determining the ignition temperature

Material	Ignition Temperature
White Phosphorus	35 degree Celsius
Petrol	246 degree Celsius
Kerosene	220 degree Celsius
Diesel	210 degree Celsius
Wood	300 degree Celsius
Coal	454 degree Celsius
Piece of paper	233 degree Celsius

Thermogravimetric analysis or **thermal gravimetric analysis** (TGA) is a method of thermal analysis in which the mass of a sample is measured over time as the temperature changes.



COMBUSTION MODEL – 1 layer

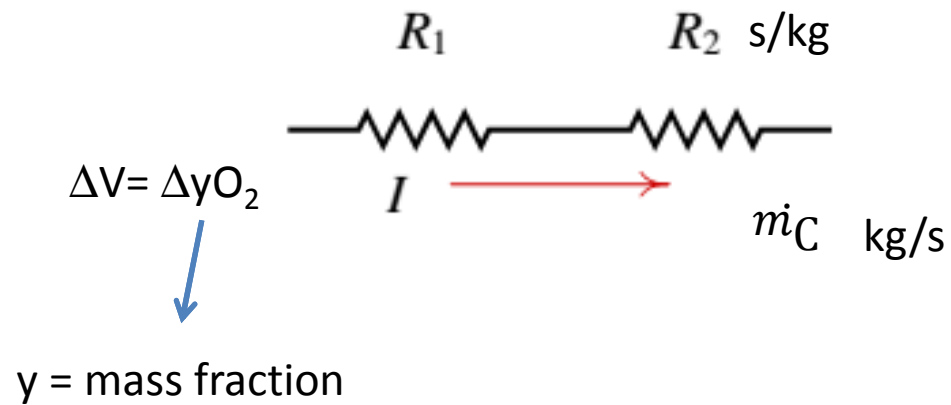


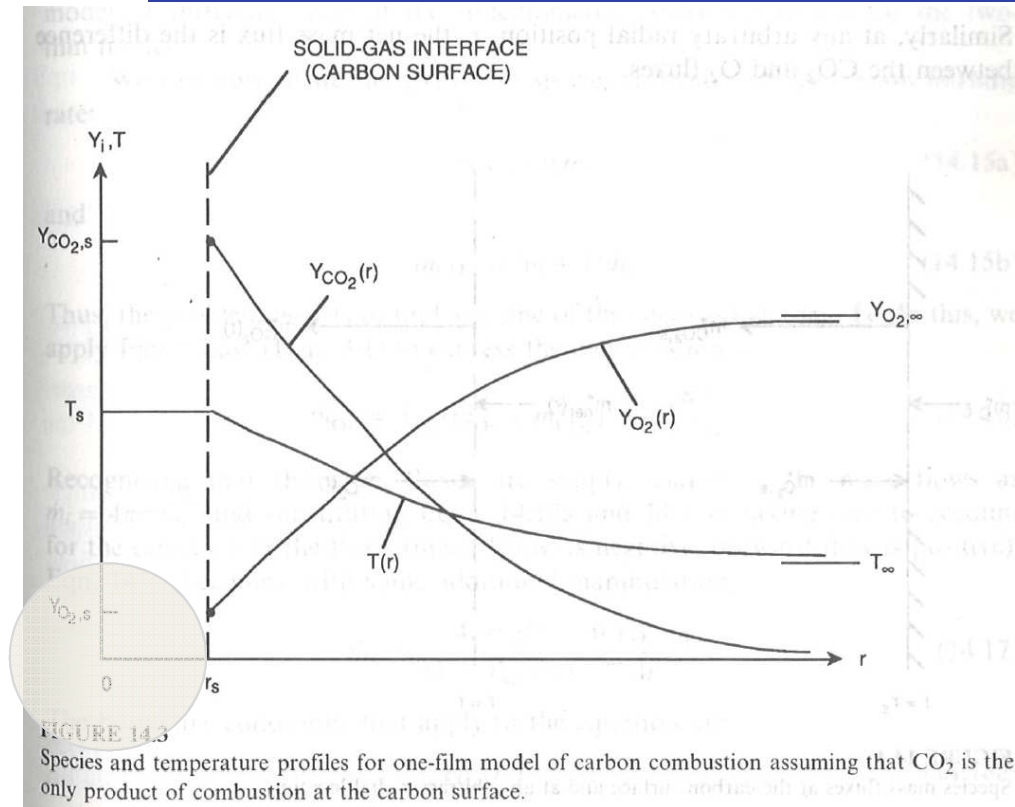
$$R_{kin} = \frac{M_{O_2} R T_s}{4\pi r_s^2 k_c M_C M_{mist} \rho}$$

Kinetic
mechanism

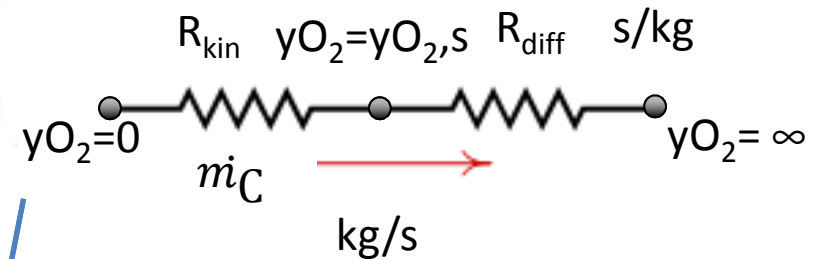
$$R_{diff} = \frac{s + y_{O_2, s}}{4\pi r_s \rho D^M}$$

Diffusion
mechanism





COMBUSTION MODEL – 1 layer



y = mass fraction

$$R_{kin} = \frac{s}{4\pi r_s^2 \rho k_c} \xrightarrow{\text{A.exp } (-E_A/R.T_s)} \text{Kinetic rate} \sim 3 \cdot 10^5 \exp(-17966/T_s) \text{ m/s}$$

$\searrow$
 Mixture density $\rho = P/(R/M \cdot T)$
 Mixture molar mass $\sim 29 \text{ kg/kmol}$

$$s = M_{O_2}/MC$$

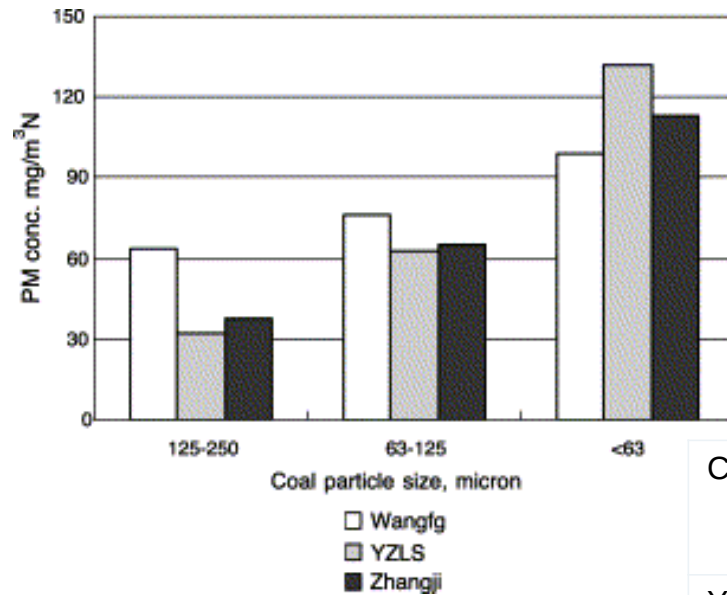
$$R_{diff} = \frac{s + y_{O_2} s}{4\pi r_s \rho D^M} \xrightarrow{\quad} \text{Diffusion rate} \sim 1.2 \cdot 10^{-4} \text{ m}^2/\text{s}$$

$\downarrow$
 0.5 x Particle Diameter

Time for burning = D^2/K_B

$$K_B = \frac{8\rho D^M}{\rho_C} \ln\left(1 + \frac{y_{O_2,\infty}}{s}\right)$$

Residence time in the boiler is typically 2-5 seconds



**Less coal particle size
more PM emissions**

<http://www.sciencedirect.com/science/article/pii/S0378382003003060>

Coal type	Coal particle size, μm	Ultimate analysis, wt.%, daf			
		C	H	N	S+O ^a
YZLS	125–250	81.89	5.59	2.31	10.20
	63–125	80.13	5.30	2.08	12.49
	<63	79.45	5.10	2.07	13.37
Zhangji	125–250	81.46	5.97	1.88	10.69
	63–125	80.15	5.64	1.68	12.53
	<63	79.58	5.50	1.73	13.19
Wangfg	125–250	85.60	5.38	2.13	6.89
	63–125	87.96	6.06	2.19	3.79
	<63	88.52	5.48	2.22	3.79

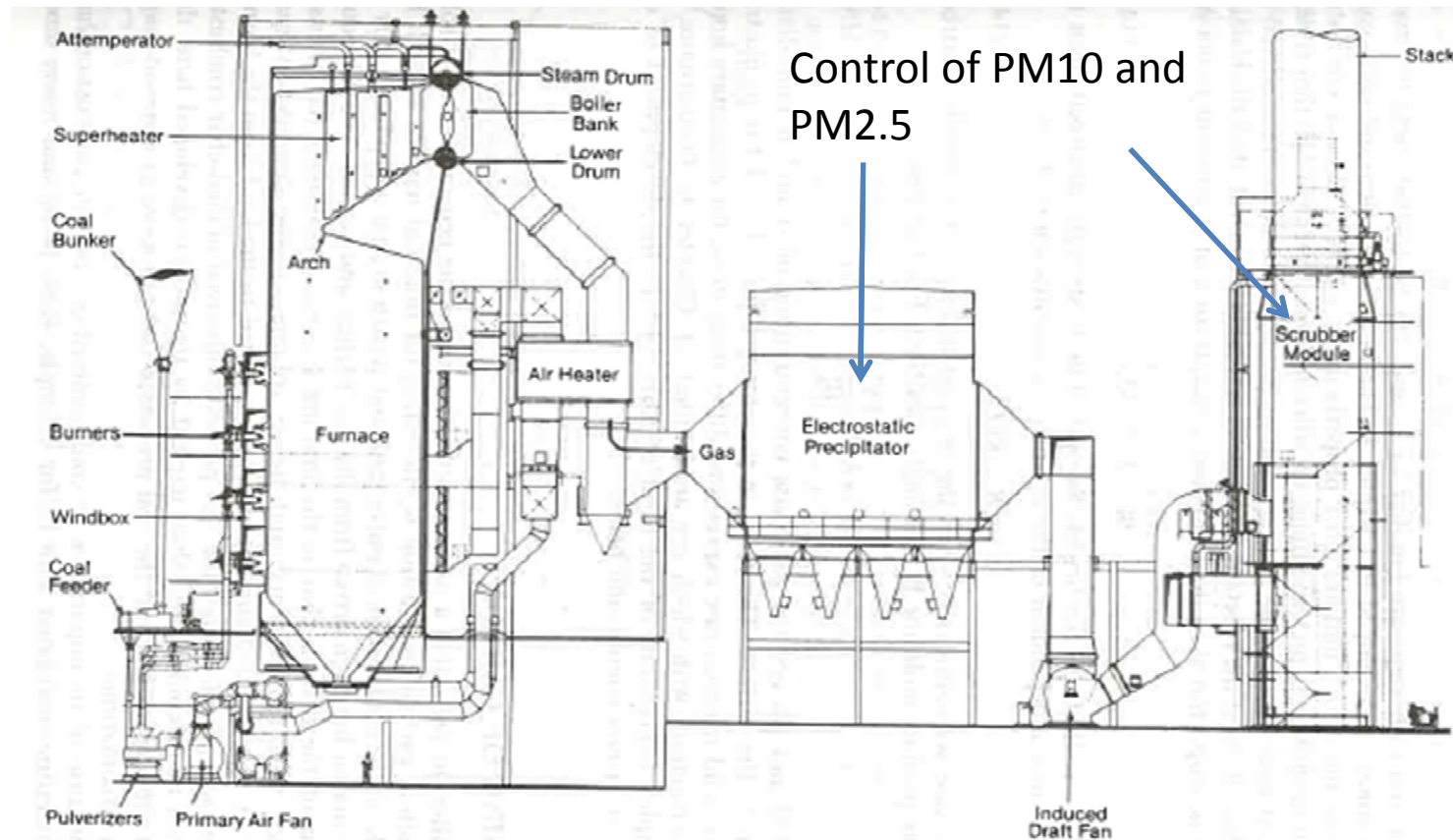


FIGURE 14.1

Pulverized-coal boiler. (Reprinted from Ref. [1] with permission of Babcock and Wilcox Co.)

Scrubber “Spray tower”

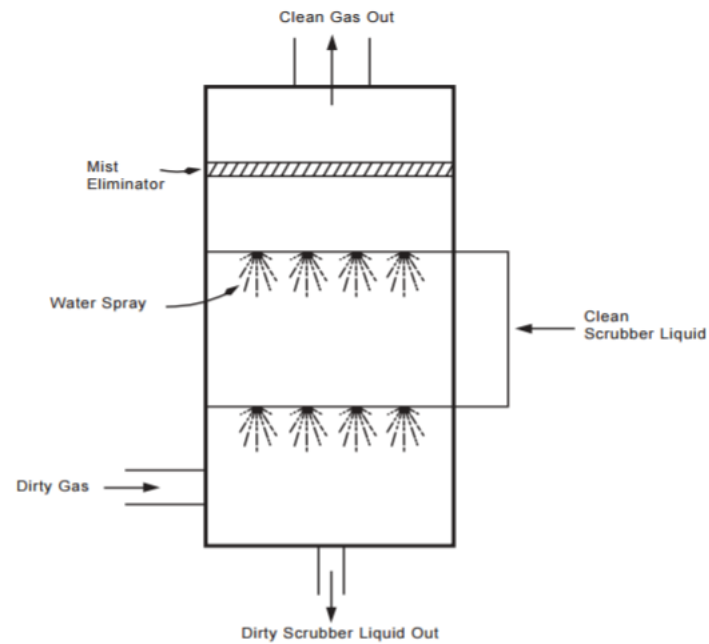


Figure 2.1: Spray Tower [4]

“Cyclonic Spray”

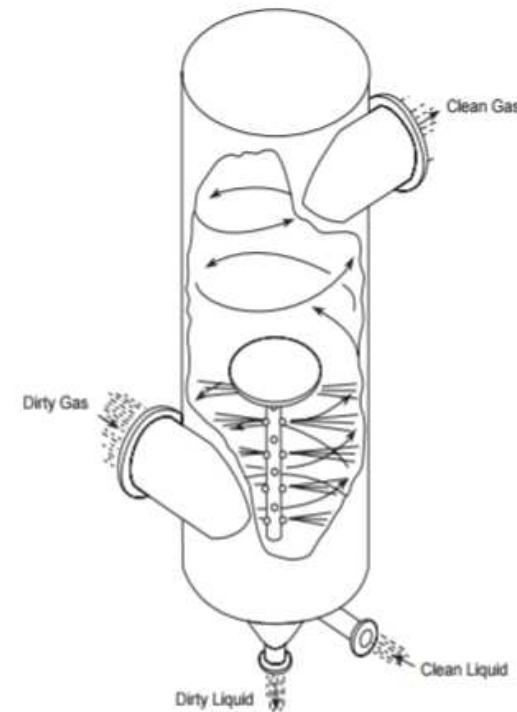
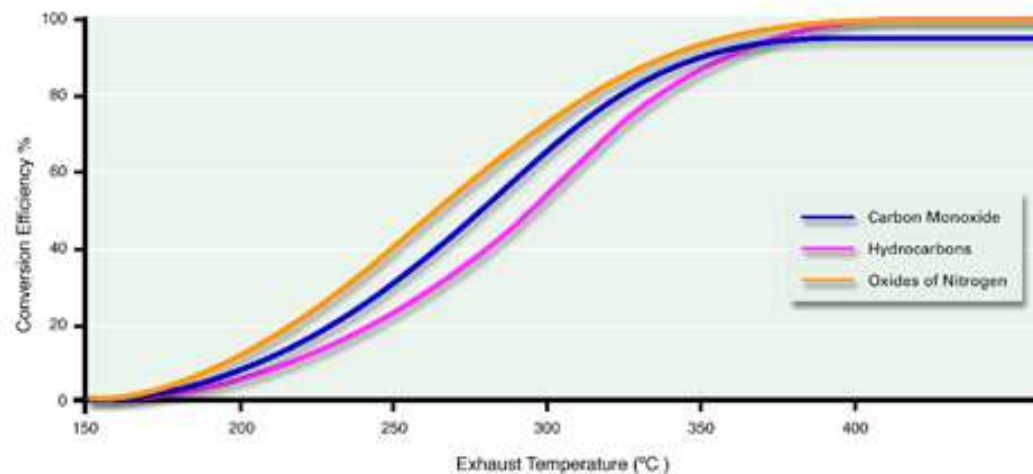


Figure 2.2: Cyclonic Spray Scrubber [3]

**Combustion of coal main
pollutants:
NOx and PM!!!**

P#13 A mixture of methane gas and air at 25°C and 1 atm is burned in a water heater at 100% theoretical air. The mass flow rate of methane is 1.15 kg/h. The exhaust gas temperature was measured to be 500 °C and approximately 1 atm and is subjected to exhaust aftertreatment. The volumetric flow rate of cold water (at 22 °C) to the heater is 4 L/min.

Effect of temperature on the operation of a three-way catalytic converter (Lambda= 1)



- Determine the combustion efficiency.
- Calculate the temperature of the hot water if the heat exchanger were to have an efficiency of 1.0, i.e., perfect heat transfer.
- Consider the following concentrations of emissions at the combustion products: 5000 ppm NO. Estimate the NO exhaust gas emissions in g/h.

P#14 (exercício 12.4 livro Português) Uma caldeira de uma central termoe elétrica é alimentada com um fuel-óleo residual que apresenta a seguinte composição mássica elementar indicada na tabela. Considerando combustão completa com 25% de excesso de ar,

- Estime a relação (A/F)_{st}.
- Estime a concentração mássica de SO₂ nos produtos de combustão.
- Compare com o limite seco a 3% de O₂ de 200 mg/Nm³.
- Pode estimar a concentração de partículas no escape? Como?

C	86.4%
H	9.8%
N	0.35%
S	1.13%
O	2.28%
Cinzas/Ash	0.04%

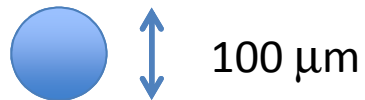
Combustion in solids

P#15 Using a one layer coal combustion model estimate the combustion rate of the coal particles. An the time of burning.

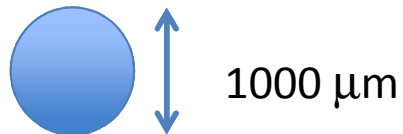
$T_s \sim 1500 \text{ K}$



i) Combustion rate kg/s ????



ii) In what time ??????

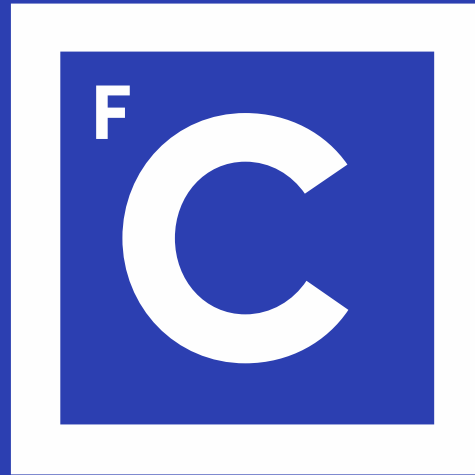


iii) Estimate the minimum residence time in the boiler for combustion of all coal particles.

$\rho_c \sim 1900 \text{ kg/m}^3$

The image consists of a large blue square. Inside this square is a white square border. Within the white border is a smaller blue square. The word "Obrigado" is written in white, bold, sans-serif font in the center of the inner blue square.

Obrigado



Ciências ULisboa

Faculdade
de Ciências
da Universidade
de Lisboa